

# Onde acoustique avec changement de phase induit

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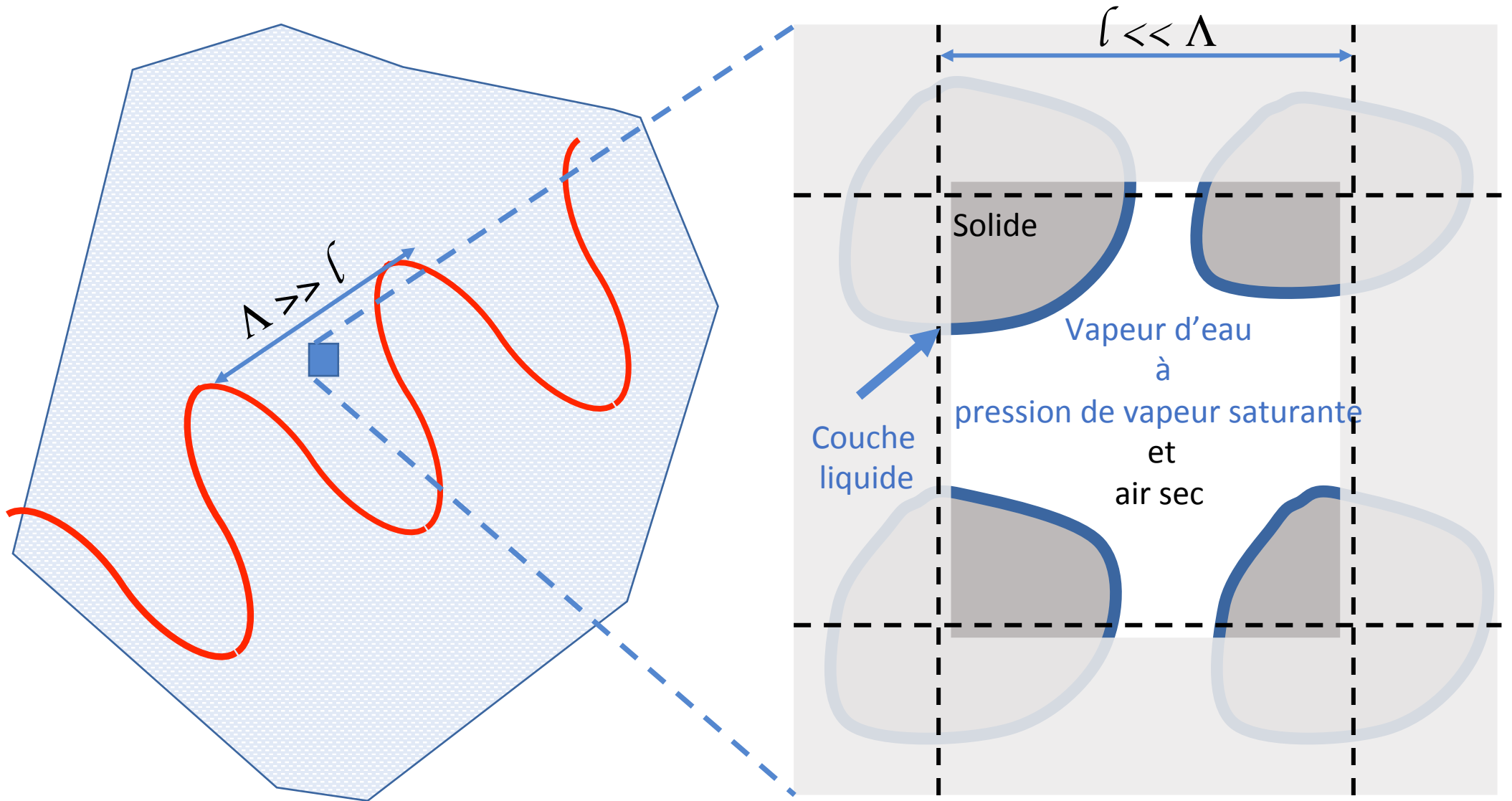
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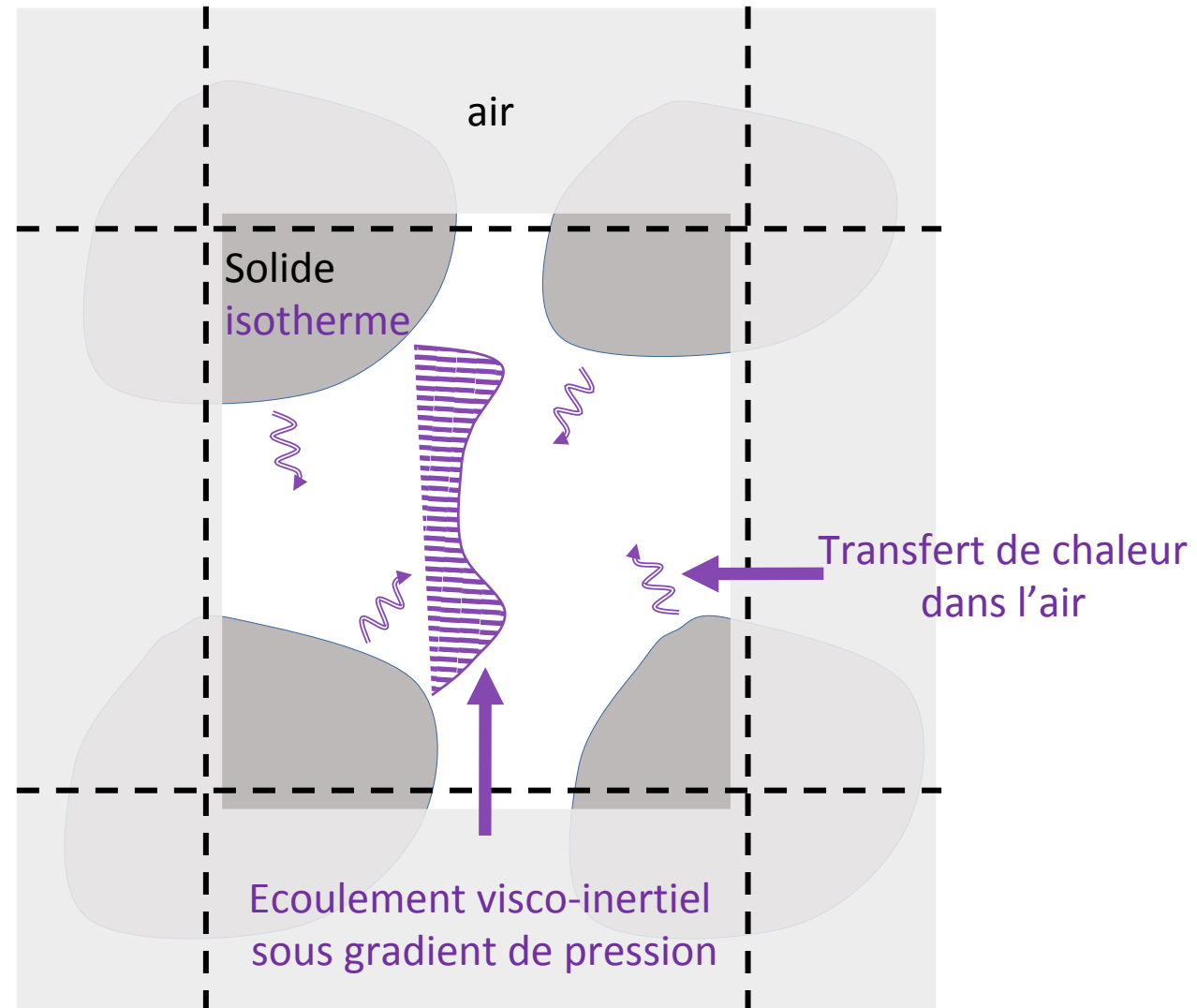
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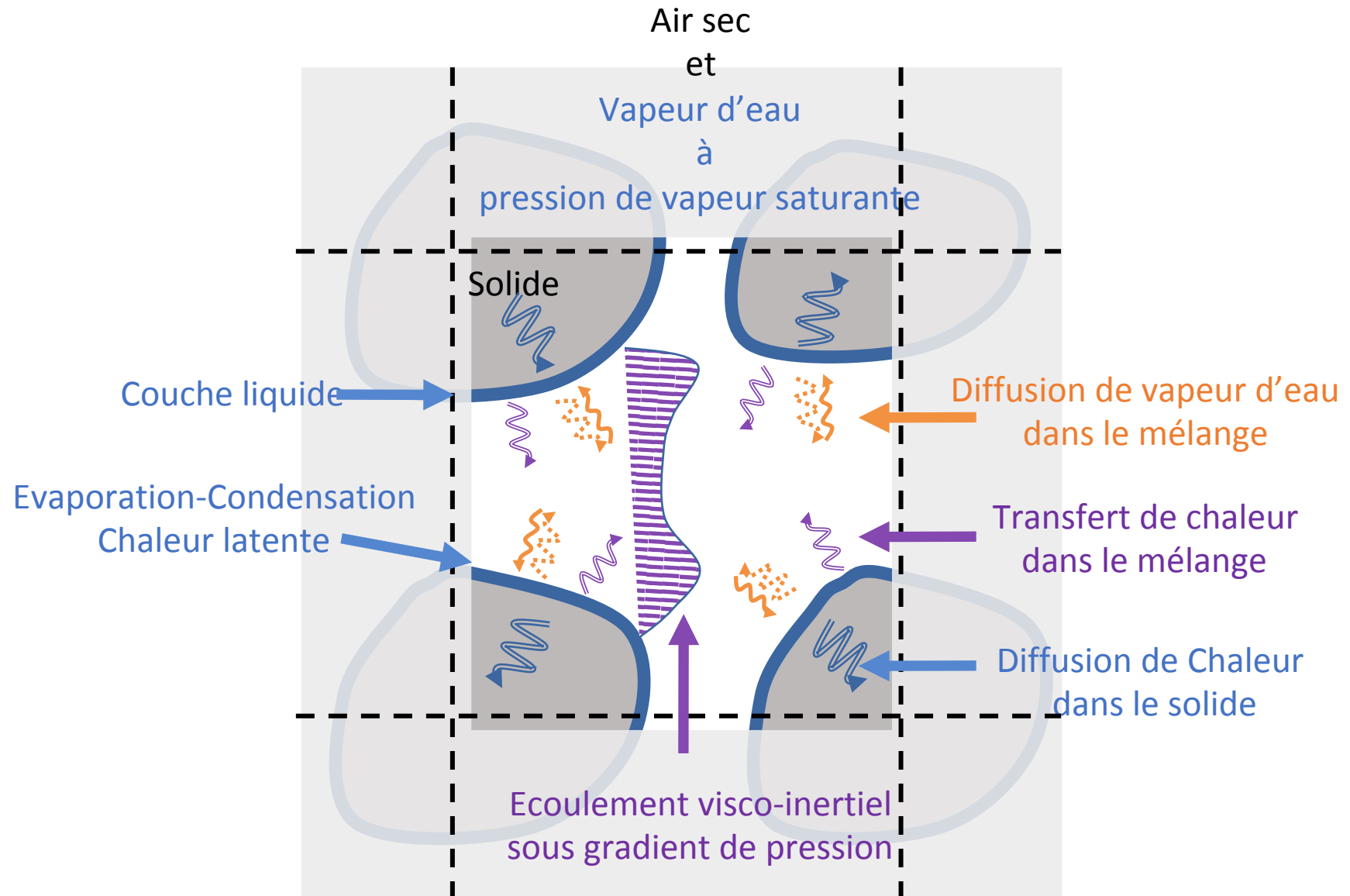
# Acoustique en Milieu poreux humide



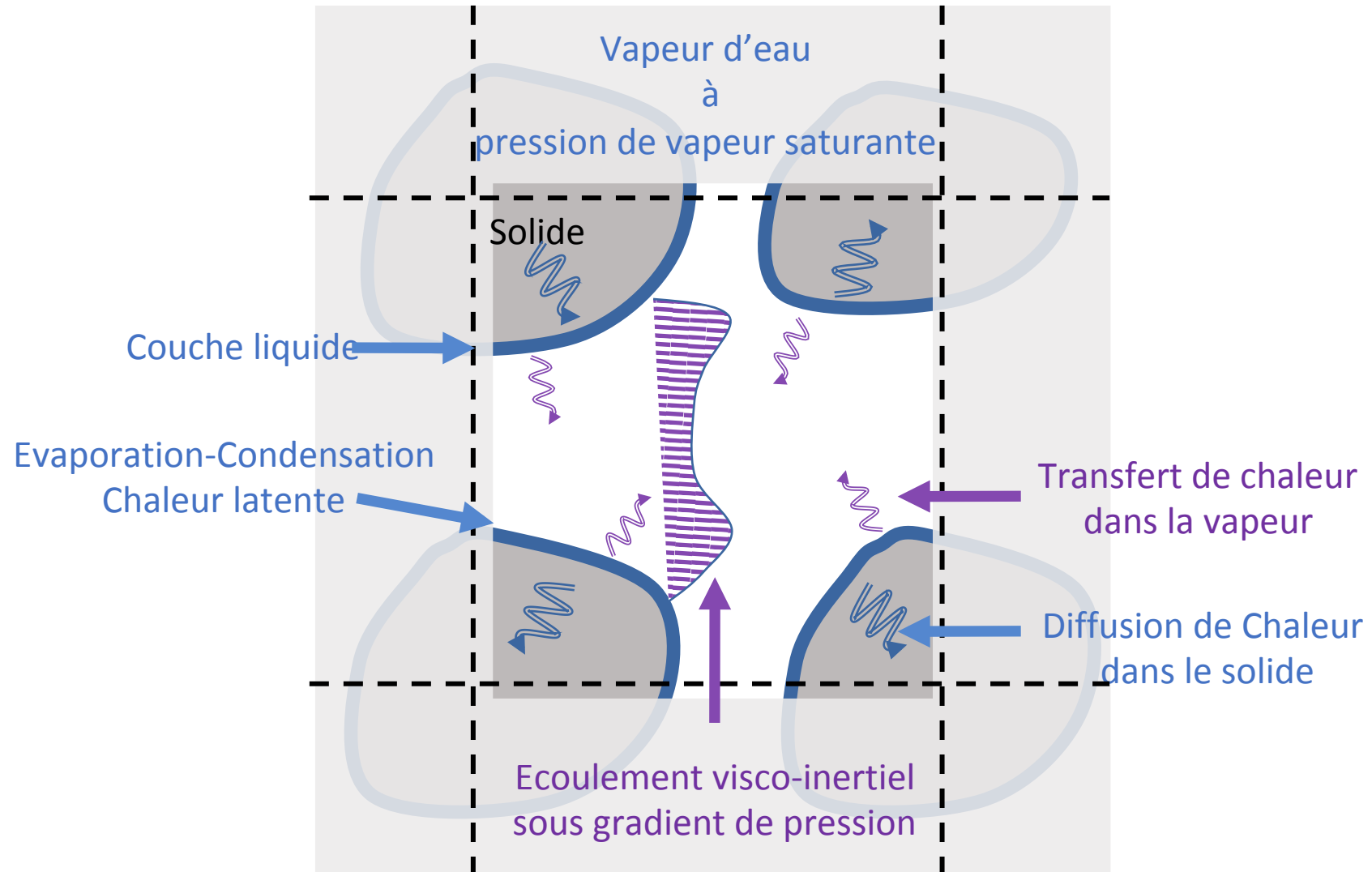
# Physique des ondes en milieu sec



# Physique en milieu humide



# Milieu saturé en vapeur d'eau



# Le système d'équations classique

Perturbation en régime harmonique  $e^{+i\omega t}$

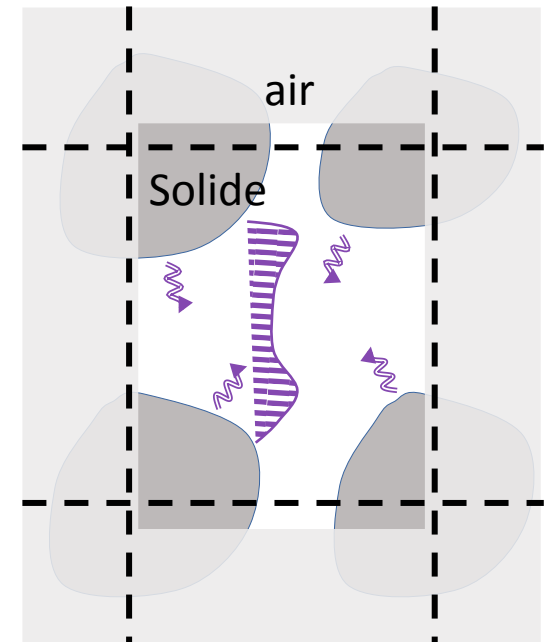
$$\mathbf{div}(\boldsymbol{\sigma}) = i\omega\rho^e\mathbf{v}$$

$$\boldsymbol{\sigma} = 2\eta\mathbf{D}(\mathbf{v}) - p\mathbf{I}$$

$$\rho^e\mathbf{div}(\mathbf{v}) + i\omega\rho = 0$$

$$-\mathbf{div}(\kappa\mathbf{grad}\tau) + i\omega\rho^e c_p\tau = i\omega p$$

$$\frac{p}{Pe} = \frac{\rho}{\rho^e} + \frac{\tau}{Te}$$



# Les équations de changement de phase

## Clapeyron et chaleur latente $\mathcal{L}$

! 
$$\tau = \tau_w = \tau_\Gamma = p_v \frac{T^e}{\mathcal{L} \rho_v^e}$$

! 
$$(-\kappa_w \mathbf{grad} \tau_w + \kappa \mathbf{grad} \tau) \cdot \mathbf{n} = -\mathcal{L} \mathbf{j} \cdot \mathbf{n}$$

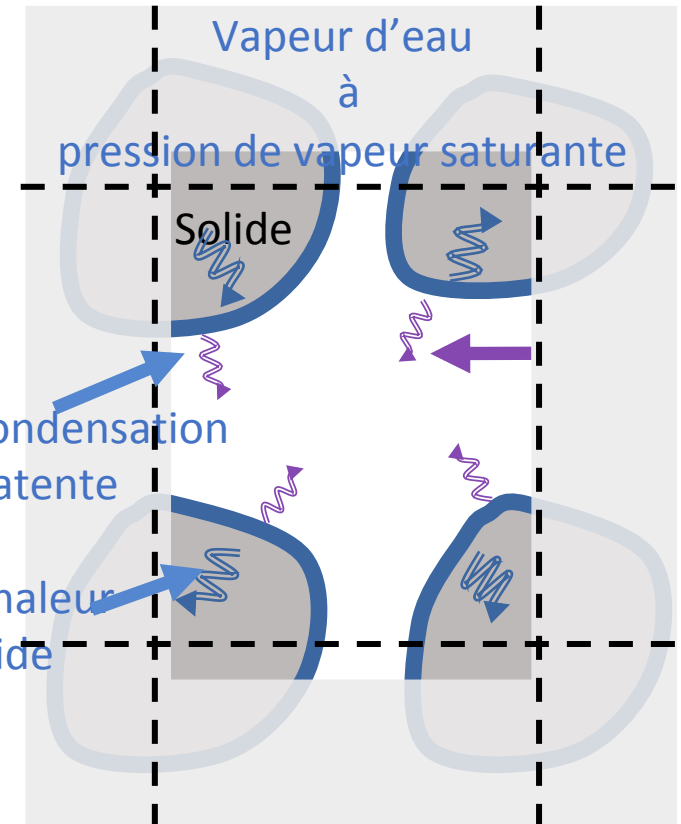
$$-\text{div}(\kappa_{ws} \mathbf{grad} \tau_{ws}) + i\omega(\rho c)_{ws} \tau_{ws} = 0$$

## Vitesse à l'interface $\Gamma$

$$\mathbf{v}_w = \mathbf{0}$$

$$(\mathbf{v} - \mathbf{v}_w) \cdot \mathbf{n} = \left( \frac{1}{\rho_v^e} - \frac{1}{\rho_w} \right) \mathbf{j} \cdot \mathbf{n}$$

! 
$$\mathbf{v} \cdot \mathbf{n} = \frac{1}{\rho_v^e} \mathbf{j} \cdot \mathbf{n}$$



**Analyse physique**  $\varepsilon = \frac{l}{L} \ll 1$

**Acoustique à grande longueur d'onde :  $L = \Lambda/2\pi$**

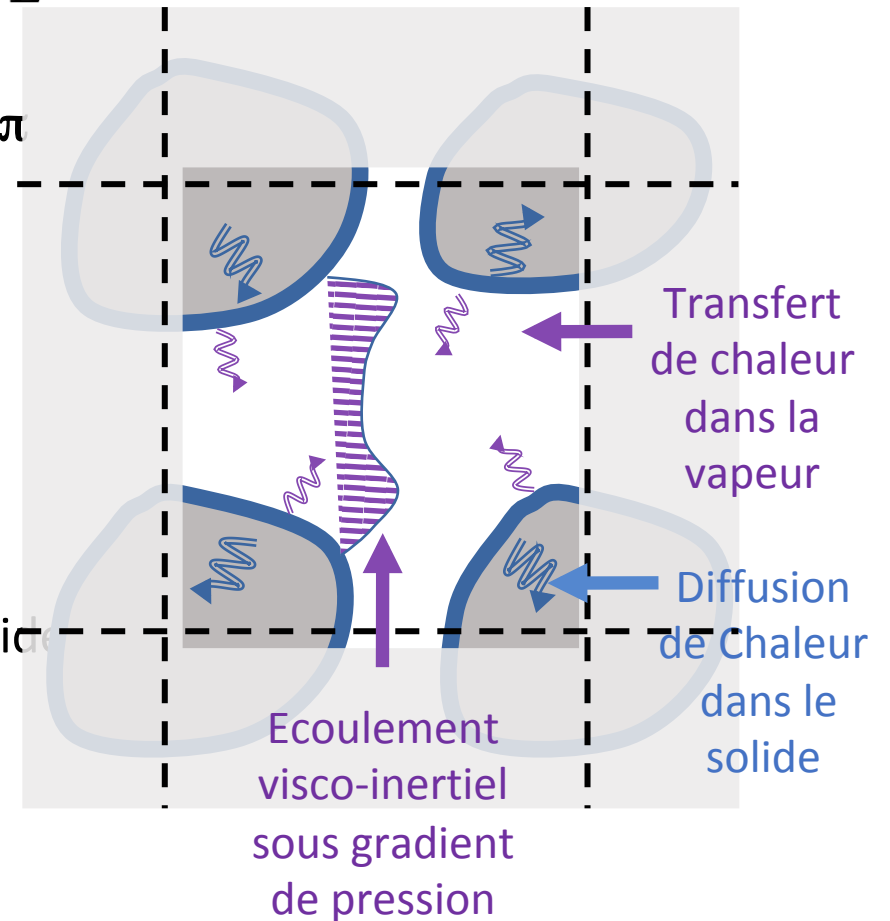
$$\text{grad}(p) = O\left(\frac{p}{L}\right) \quad ; \quad \text{div}(\mathbf{v}) = O\left(\frac{v}{L}\right)$$

**Quantités oscillant à l'échelle des pores :  $l \ll \Lambda/2\pi$**

Temperature  
Vitesse  
Masse volumique

**Contrastes**

Conductivité thermique vapeur  $\ll$  eau/solide  
Masse volumique vapeur  $\ll$  eau  
Vitesse sur  $\Gamma \ll$  Vitesse dans  $\Omega_g$





# Homogénéisation

Procédure usuelle par développement asymptotique  
en  
puissance de  $\varepsilon$   
des  
variables exprimées en double échelle  $x, y = \varepsilon^{-1}x$

## Systeme renormalisé en double échelles $\mathbf{x}, \mathbf{y} = \varepsilon^{-1}\mathbf{x}$

in  $\Omega_g$

$$-\varepsilon^2 \operatorname{div}(\kappa \operatorname{grad} \tau) + i\omega \rho^e c_p \tau = i\omega p$$

$$\rho^e \operatorname{div}(\mathbf{v}) + i\omega \rho = 0$$

$$-\varepsilon^2 \operatorname{div}(\kappa \operatorname{grad} \tau) + i\omega \rho^e c_p \tau = i\omega p$$

$$\frac{p}{Pe} = \frac{\rho}{\rho^e} + \frac{\tau}{T^e}$$

in  $\Omega_{ws}$

$$-\varepsilon^2 \operatorname{div}(\kappa_{ws} \operatorname{grad} \tau_{ws}) + i\omega (\rho c)_{ws} \tau_{ws} = 0$$

on  $\Gamma$

$$(-\varepsilon \kappa_w \operatorname{grad} \tau_w + \varepsilon^2 \kappa \operatorname{grad} \tau) \cdot \mathbf{n} = -\mathcal{L} \mathbf{j} \cdot \mathbf{n}$$

$$\mathbf{v} \cdot \mathbf{n} = \varepsilon \frac{1}{\rho_v^e} \mathbf{j} \cdot \mathbf{n}$$

$$\Delta_x(q) = O\left(\frac{q}{L^2}\right) = O\left(\frac{q}{L^2}\right) \frac{\ell^2}{L^2} = O\left(\frac{q}{\ell^2}\right) \varepsilon^2$$

$$\kappa \operatorname{grad} \tau \cdot \mathbf{n} \ll -\kappa_w \operatorname{grad} \tau_w \approx \mathcal{L} \mathbf{j} \cdot \mathbf{n}$$

$$d(S\rho^e|v|)/S\rho^e|v| \approx \ell/L = \varepsilon$$

$$d(S\rho^e|v|) \approx |j|\Gamma$$

$$|v|_{\Gamma}/|v| \approx |j|_{\Gamma}/S\rho^e|v| \approx \ell/L = \varepsilon$$

# Loi de Darcy dynamique

Ordre dominant

$$\text{grad}_y p^{(0)} = 0 \quad ; \quad p^{(0)} = P(\mathbf{x})$$

Ordre suivant

$$-\text{grad}_y p^{(1)} - \text{grad}_x P + \eta \Delta_y \mathbf{v}^{(0)} = i\omega \rho^e \mathbf{v}^{(0)}$$

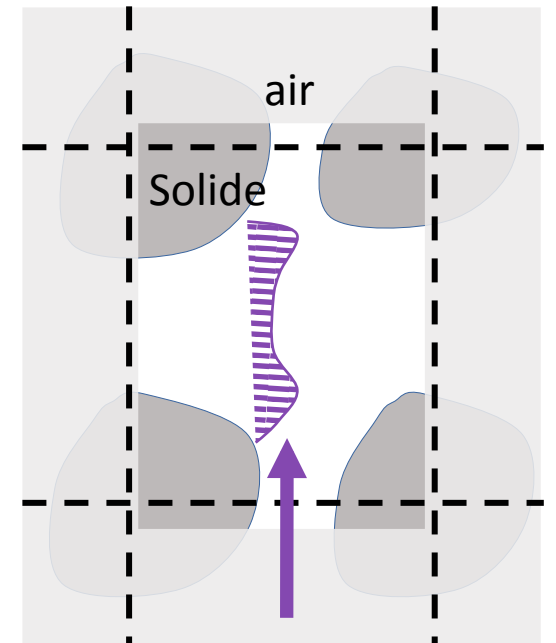
$$\text{div}_y(\mathbf{v}^{(0)}) = 0$$

$$\mathbf{v}^{(0)} = \mathbf{0}$$

$$p^{(1)}; \mathbf{v}^{(0)} : \Omega - \text{periodic}$$

Résolution classique

$$\mathbf{v}^{(0)}(\mathbf{x}, \mathbf{y}) = -\mathbf{k}(\omega, \mathbf{y}) \text{grad}_x P \quad \text{soit} \quad \boxed{V(\mathbf{x}) = \langle \mathbf{v}^{(0)} \rangle = -\mathbf{K}(\omega) \text{grad}_x P}$$



Écoulement visco-inertiel  
sous gradient de pression

Le changement de phase n'affecte pas la loi de Darcy dynamique

# Température d'interface eau-vapeur

Equilibre liquide vapeur : Relation de Clapeyron

$$\tau^{(0)} = \tau_w^{(0)} = T_\Gamma(\mathbf{x}) = P(\mathbf{x}) \frac{T^e}{\mathcal{L}\rho_v^e} \quad \text{on } \Gamma$$

**!** Uniforme  $\neq 0$  sur  $\Gamma$

# Vapeur - Transfert thermique

## Ordre dominant

$$-\operatorname{div}_y(\kappa \operatorname{grad}_y \tau^{(0)}) + i\omega \rho^e c_p \tau^{(0)} = i\omega P \quad \text{in } \Omega_g$$

$$\tau^{(0)} = T_\Gamma \quad \text{on } \Gamma$$

$$\tau^{(0)} : \Omega - \text{periodic}$$

## Résolution classique $\tilde{\tau} = \tau^{(0)} - T_\Gamma$

$$-\operatorname{div}_y(\kappa \operatorname{grad}_y \tilde{\tau}) + i\omega \rho^e c_p \tilde{\tau} = i\omega(P - \rho^e c_p T_\Gamma) \quad \text{in } \Omega_g$$

$$\tilde{\tau} = 0 \quad \text{on } \Gamma$$

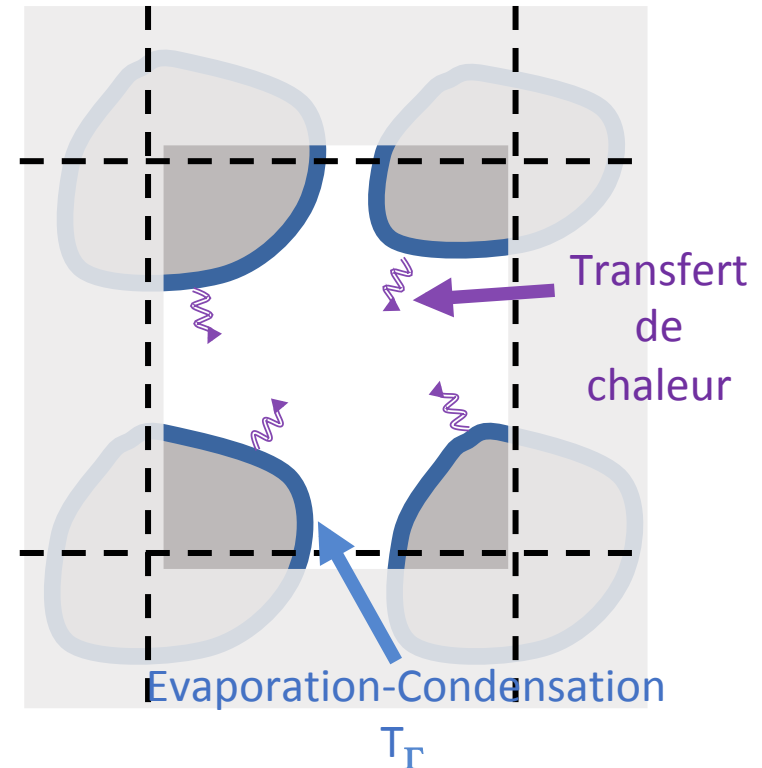
$$\tilde{\tau} : \Omega - \text{periodic}$$

## Solution particulière complexe

$$-\operatorname{div}_y(\operatorname{grad}_y \theta) - \frac{i\omega \rho^e c_p}{\kappa} \theta = 1 \quad \text{in } \Omega_g$$

$$\theta = 0 \quad \text{on } \Gamma$$

$$\theta : \Omega - \text{periodic}$$



# Vapeur - Température et masse volumique

Température

$$\tau^{(0)} = T_{\Gamma} + \left( \frac{P}{\rho^e c_p} - T_{\Gamma} \right) \frac{i\omega \rho^e c_p \theta(\mathbf{y})}{\kappa}$$

Masse volumique

$$\frac{\rho^{(0)}}{\rho^e} = \frac{P}{P^e} - \frac{\tau^{(0)}}{T^e} = \frac{P}{P^e} - \frac{T_{\Gamma}}{T^e} - \left( \frac{P}{\rho^e c_p T^e} - \frac{T_{\Gamma}}{T^e} \right) \frac{i\omega \rho^e c_p \theta(\mathbf{y})}{\kappa}$$

$$\left\langle \frac{\rho^{(0)}}{\rho^e} \right\rangle = \frac{P}{P^e} - \frac{T_{\Gamma}}{T^e} - \left( \frac{P}{\rho^e c_p T^e} - \frac{T_{\Gamma}}{T^e} \right) \frac{i\omega \rho^e c_p \langle \theta \rangle}{\kappa}$$

# Systeme eau & solide - Transfert thermique

## Ordre dominant

$$-\operatorname{div}_y(\kappa_{ws} \operatorname{grad}_y \tau_{ws}^{(0)}) + i\omega(\rho c)_{ws} \tau_{ws}^{(0)} = 0 \quad \text{in } \Omega_{ws}$$

$$\tau_{ws}^{(0)} = T_\Gamma \quad \text{on } \Gamma$$

$$\kappa_{ws} \operatorname{grad}_y \tau_{ws}^{(0)} \cdot n \quad \text{and} \quad \tau_{ws}^{(0)} : \text{continuous on } \Gamma_{ws}$$

$$\tau_{ws}^{(0)} : \Omega - \text{periodic}$$

## Résolution

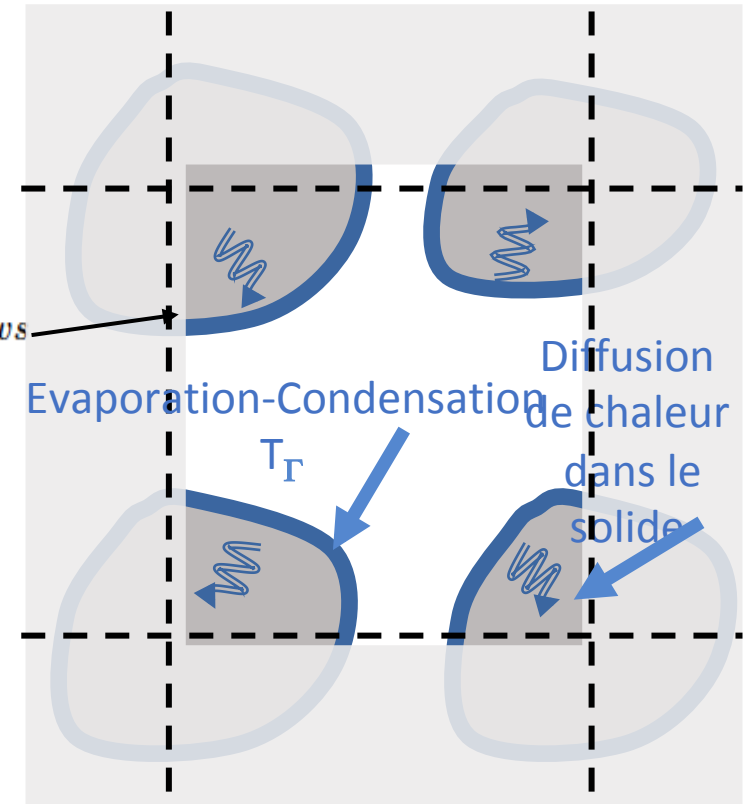
$$\tau_{ws}^{(0)} = T_\Gamma \left( 1 - i\omega \langle \rho c \rangle_{ws} \frac{\Theta(\mathbf{y})}{\kappa_w} \right)$$

## Solution particulière complexe $\Omega$ -periodic

$$-\operatorname{div}_y \left( \frac{\kappa_{ws}}{\kappa_w} \operatorname{grad}_y \Theta \right) + \frac{i\omega(\rho c)_{ws}}{\kappa_w} \Theta = \frac{(\rho c)_{ws}}{\langle \rho c \rangle_{ws}} \quad \text{in } \Omega_{ws},$$

$$\Theta = 0 \quad \text{on } \Gamma$$

$$\kappa_{ws} \operatorname{grad}_y \Theta \cdot n \quad \text{and} \quad \Theta : \text{continuous on } \Gamma_{ws}$$



# Flux de masse changeant de phase

Température

$$\tau_{ws}^{(0)} = T_{\Gamma} \left( 1 - i\omega \langle \rho c \rangle_{ws} \frac{\Theta(\mathbf{y})}{\kappa_w} \right)$$

Flux local de chaleur

$$-\mathcal{L} \mathbf{j}^{(0)} \cdot \mathbf{n} = -\kappa_w \mathbf{grad}_y \tau_w^{(0)} \cdot \mathbf{n}$$

Masse changeant de phase dans  $\Omega$

$$\begin{aligned} \int_{\Gamma} \mathbf{j}^{(0)} \cdot \mathbf{n} ds &= \frac{1}{\mathcal{L}} \int_{\Gamma} \kappa_w \mathbf{grad}_y \tau_w^{(0)} \cdot \mathbf{n} ds \\ &= \frac{1}{\mathcal{L}} \int_{\Omega_{ws}} i\omega (\rho c)_{ws} \tau_{ws}^{(0)} dv = \frac{T_{\Gamma}}{\mathcal{L}} i\omega \langle \rho c \rangle_{ws} \left( 1 - \frac{i\omega \langle \rho c \Theta \rangle_{ws}}{\kappa_w} \right) \Omega_{ws} \end{aligned}$$



# Conservation de la masse

Ordre dominant : incompressibilité  $\text{div}_y(\mathbf{v}^{(0)}) = 0$

Premier ordre  $\mathbf{v}^{(1)} \cdot \mathbf{n} = \frac{1}{\rho^e} \mathbf{j}^{(0)} \cdot \mathbf{n}$  on  $\Gamma$

$$\text{div}_y(\mathbf{v}^{(1)}) + \text{div}_x(\mathbf{v}^{(0)}) + i\omega \frac{\rho^{(0)}}{\rho^e} = 0 \text{ in } \Omega_g$$

Par intégration

$$\int_{\Omega_g} \text{div}_y(\mathbf{v}^{(1)}) dv + \int_{\Omega_g} \text{div}_x(\mathbf{v}^{(0)}) dv + \int_{\Omega_g} i\omega \frac{\rho^{(0)}}{\rho^e} dv = 0$$

$$\frac{1}{\Omega_g} \int_{\Gamma} \frac{1}{\rho^e} \mathbf{j}^{(0)} \cdot \mathbf{n} ds + \text{div}_x(\mathbf{V}) + i\omega \left\langle \frac{\rho^{(0)}}{\rho^e} \right\rangle = 0$$

# Compressibilité effective

Rappel expressions de  $T_\Gamma$ ,  $\rho$  et  $j$

$$\frac{T_\Gamma}{T^e} = \frac{P}{P^e} \frac{P^e}{\mathcal{L}\rho_v^e}$$

$$\left\langle \frac{\rho^{(0)}}{\rho^e} \right\rangle = \frac{P}{P^e} - \frac{T_\Gamma}{T^e} - \left( \frac{P}{\rho^e c_p T^e} - \frac{T_\Gamma}{T^e} \right) \frac{i\omega \rho^e c_p \langle \theta \rangle}{\kappa}$$

$$\frac{1}{\Omega_g} \int_\Gamma \frac{1}{\rho_v^e} \mathbf{j}^{(0)} \cdot \mathbf{n} ds = i\omega \frac{T_\Gamma}{\mathcal{L}\rho_v^e} \langle \rho c \rangle_{ws} \left( 1 - \frac{i\omega \langle \rho c \theta \rangle_{ws}}{\kappa_w} \right) \frac{\Omega_{ws}}{\Omega_g}$$

Effet de changement de phase

$$\text{div}_x(\mathbf{V}) = -i\omega \frac{P}{P^e} \left( 1 - \frac{P^e}{\mathcal{L}\rho_v^e} \left( 1 + \left( \frac{\mathcal{L}\rho_v^e}{\rho^e c_p T^e} - 1 \right) \frac{i\omega \rho^e c_p \langle \theta \rangle}{\kappa} \right) \right)$$

$$-i\omega \frac{P}{P^e} \left( \frac{P^e T^e \langle \rho c \rangle_{ws}}{(\mathcal{L}\rho_v^e)^2} \left( 1 - \frac{i\omega \langle \rho c \theta \rangle_{ws}}{\kappa_w} \right) \frac{\Omega_{ws}}{\Omega_g} \right)$$

## Quantification

$$\text{div}_x(\mathbf{V}) = -i\omega \frac{P}{P^e} \left( 1 - \frac{P^e}{\mathcal{L}\rho_v^e} \left( 1 + \left( \frac{\mathcal{L}\rho_v^e}{\rho^e c_p T^e} - 1 \right) \frac{i\omega \rho^e c_p \langle \theta \rangle}{\kappa} \right) \right) - i\omega \frac{P}{P^e} \left( \frac{P^e T^e \langle \rho c \rangle_{ws}}{(\mathcal{L}\rho_v^e)^2} \left( 1 - \frac{i\omega \langle \rho c \theta \rangle_{ws}}{\kappa_w} \right) \frac{\Omega_{ws}}{\Omega_g} \right)$$

$$\mathcal{L} = 22.5 \times 10^5 \text{ J/kg}$$

$$\gamma = 1.4$$

$$\frac{P^e T^e \langle \rho c \rangle_{ws}}{(\mathcal{L}\rho_v^e)^2} = \left( \frac{P^e}{\mathcal{L}\rho_v^e} \right)^2 \frac{\langle \rho c \rangle_{ws}}{\rho^e c_p} \frac{\gamma}{\gamma - 1} \approx 8$$

$$\frac{P^e}{\mathcal{L}\rho_v^e} = 3.710^{-2}$$

$$\frac{\mathcal{L}\rho_v^e}{\rho^e c_p T^e} = \frac{\mathcal{L}\rho_v^e}{P^e} \frac{\gamma - 1}{\gamma} = 7.7$$

Parametres	Liquid	Vapor	Solid
Density $\rho^e$ [kg/m <sup>3</sup> ]	10 <sup>3</sup>	1.2	2.5 × 10 <sup>3</sup>
Bulk modulus $K$ [Pa]	2 × 10 <sup>9</sup>	1.4 × 10 <sup>5</sup>	40 × 10 <sup>9</sup>
Dynamic viscosity $\mu$ [Pa.s]	10 <sup>-3</sup>	20 × 10 <sup>-6</sup>	
Kinematic viscosity $\nu$ [m <sup>2</sup> /s]	10 <sup>-6</sup>	15 × 10 <sup>-6</sup>	
Conductivity $k$ [W/K.m]	0.6	0.026	3
Heat capacity $C_p$ [J/K.kg]	4.18 × 10 <sup>3</sup>	10 <sup>3</sup>	0.8 × 10 <sup>3</sup>
Diffusivity $d$ [m <sup>2</sup> /s]	1.4 × 10 <sup>-7</sup>	2.1 × 10 <sup>-5</sup>	1.5 × 10 <sup>-6</sup>

## Dépendance fréquentielle

$$\text{div}_x(\mathbf{V}) = -i\omega \frac{P}{P^e} \left( 1 - \frac{P^e}{\mathcal{L}\rho_v^e} \left( 1 + \left( \frac{\mathcal{L}\rho_v^e}{\rho^e c_p T^e} - 1 \right) \frac{i\omega \rho^e c_p \langle \theta \rangle}{\kappa} \right) \right) - i\omega \frac{P}{P^e} \left( \frac{P^e T^e \langle \rho c \rangle_{ws}}{(\mathcal{L}\rho_v^e)^2} \left( 1 - \frac{i\omega \langle \rho c \Theta \rangle_{ws}}{\kappa_w} \right) \frac{\Omega_{ws}}{\Omega_g} \right)$$

$$\left\{ \begin{array}{ll} \langle \theta \rangle \rightarrow \theta_0 = O(\ell_g)^2 & \text{when } \omega \ll \omega_g = \frac{\kappa}{\rho^e c_p \theta_0} \approx \frac{2.10^{-5}}{(\ell_g)^2} \\ \frac{i\omega \rho^e c_p \langle \theta \rangle}{\kappa} \rightarrow 1 & \text{when } \omega \gg \omega_g = \frac{\kappa}{\rho^e c_p \theta_0} \end{array} \right.$$

Quasi-isotherme

Quasi-adiabatique

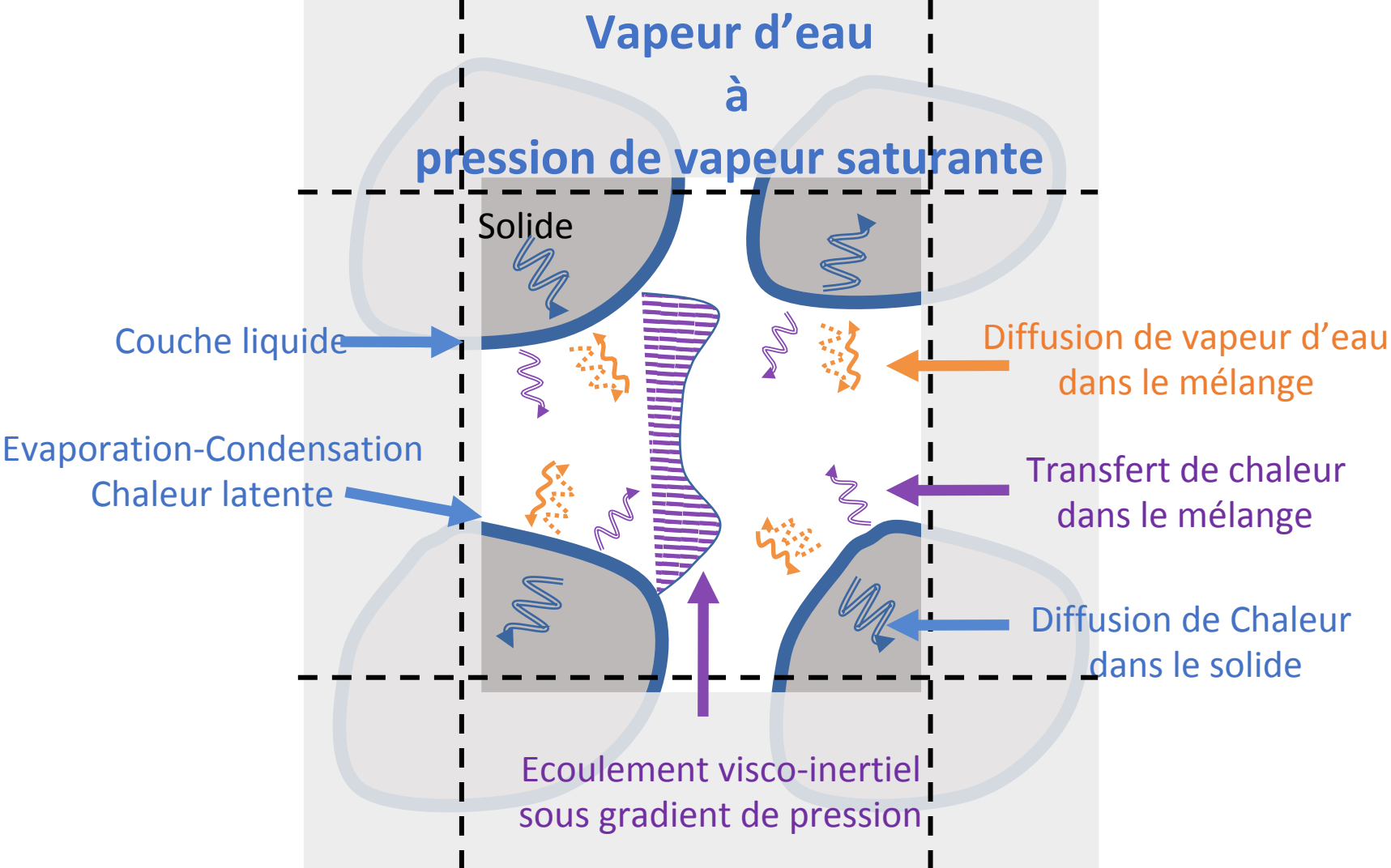
$$\left\{ \begin{array}{ll} \langle \Theta \rangle \rightarrow \Theta_0 = O(\ell_s)^2 & \text{when } \omega \ll \omega_s = \frac{\kappa_s}{(\rho^e c_p)_s \Theta_0} \approx \frac{1.510^{-6}}{(\ell_s)^2} \\ \frac{i\omega \langle \rho c \Theta \rangle_{ws}}{\kappa_w} \rightarrow 1 & \text{when } \omega \gg \omega_s = \frac{\kappa_s}{(\rho^e c_p)_s \Theta_0} \end{array} \right.$$

Compressibilité x 9

Effet négligeable

# Milieu à 100% Humidité

Air sec  
et



## Approche en Faible diffusion

Pression de vapeur saturante  $P_v^e$  à  $T^e$  :

Rankine

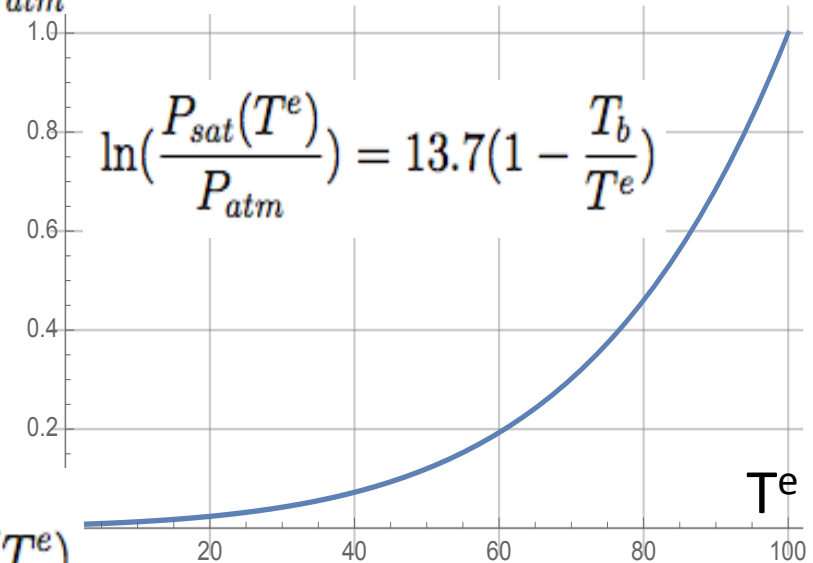
Equation d'éta  $\frac{p_v}{P_v^e} = \frac{\rho_v}{\rho_v^e} + \frac{\tau}{T^e}$

Ordre domina  $\frac{p_v^{(0)}}{P_v^e} - \frac{P}{P^e} = \frac{\rho_v^{(0)}}{\rho_v^e} - \frac{\rho^{(0)}}{\rho^e}$

Faible diffusior  $\frac{\rho_v^{(0)}}{\rho^{(0)}} = \frac{\rho_v^e}{\rho^e}$  donc  $\frac{p_v^{(0)}}{P} = \frac{P_{sat}^e}{P^e} = \frac{P_v(\mathbf{x})}{P(\mathbf{x})} = f_R(T^e)$

Clapeyron sur  $\tau^{(0)} = T_\Gamma(\mathbf{x}) = P_v(\mathbf{x}) \frac{T^e}{\mathcal{L}\rho_v^e} = f_R(T^e) P(\mathbf{x}) \frac{T^e}{\mathcal{L}\rho_v^e}$  on  $\Gamma$

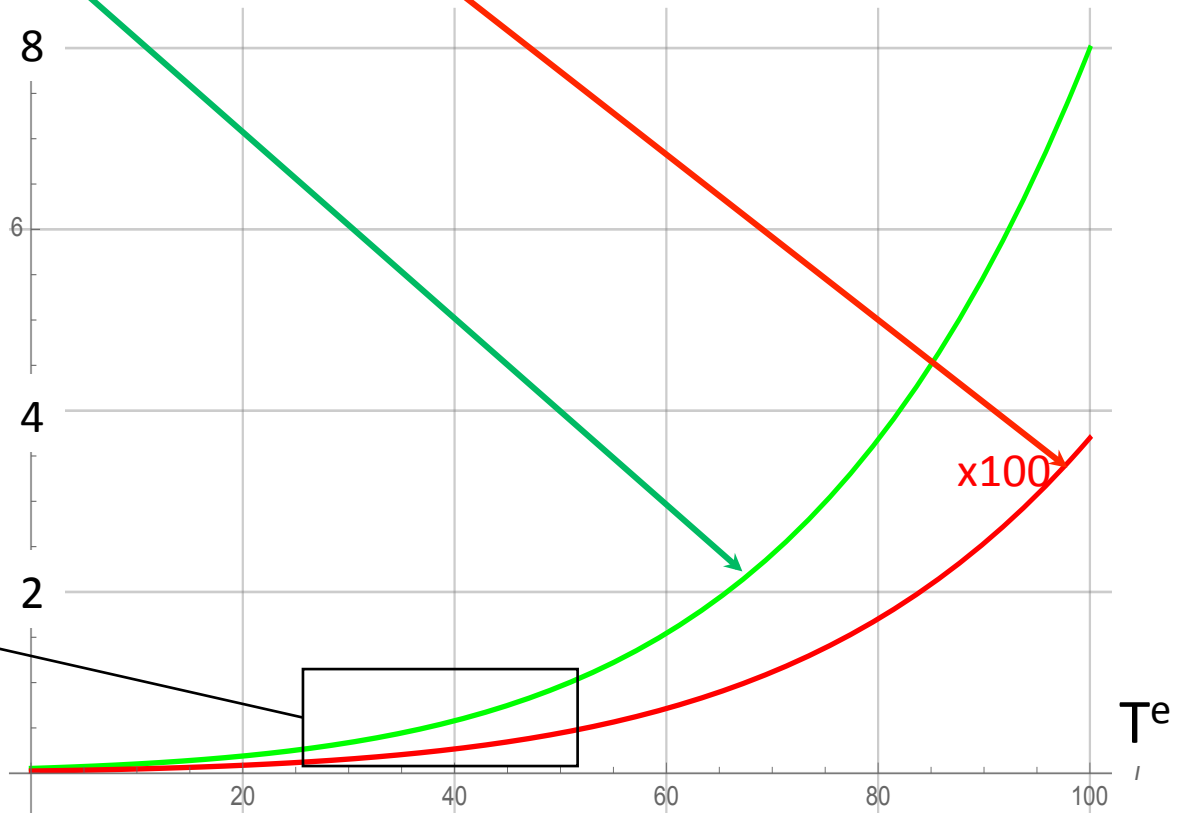
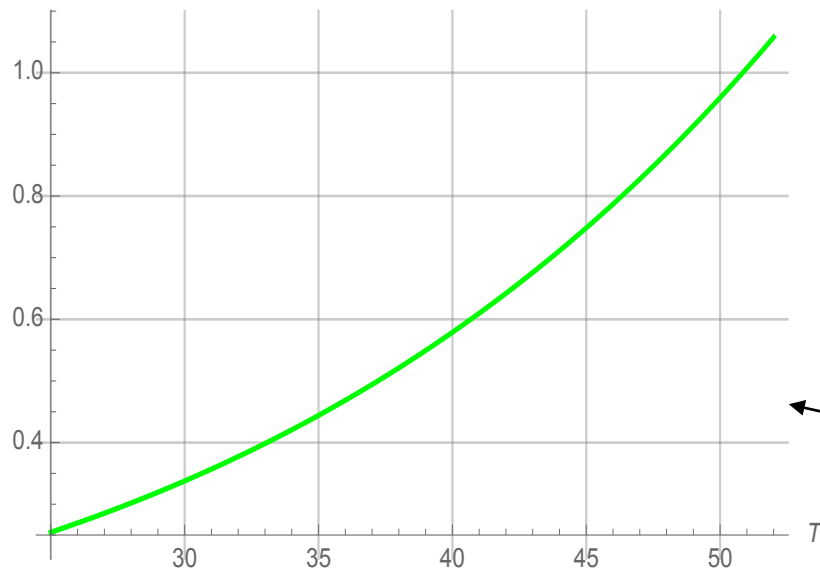
$$\frac{P_{sat}(T^e)}{P_{atm}} = f_R(T^e)$$



# Compressibilité effective à T<sup>e</sup> et 100% Humidité

$$\text{div}_x(\mathbf{V}) = -i\omega \frac{P}{P^e} \left( 1 - \frac{f_R(T^e)P^e}{\mathcal{L}\rho_v^e} \left( 1 + \left( \frac{\mathcal{L}\rho_v^e}{\rho^e c_p T^e f_R(T^e)} - 1 \right) \frac{i\omega \rho^e c_p \langle \theta \rangle}{\kappa} \right) \right) - i\omega \frac{P}{P^e} \left( \frac{f_R(T^e)P^e T^e \langle \rho c \rangle_{ws}}{(\mathcal{L}\rho_v^e)^2} \left( 1 - \frac{i\omega \langle \rho c \Theta \rangle_{ws}}{\kappa_w} \right) \frac{\Omega_{ws}}{\Omega_g} \right)$$

Effet de changement de phase selon T<sup>e</sup>



**Effet notable à forte température**

**Nette dépendance fréquentielle**

**Dissipation additionnelle**

**Rôle du solide**

**Paramètres adimensionnels du phénomène**

**Confrontation expérimentale ?**

**Intégrer la diffusion vapeur-air ?**

## **Conclusion**





## Quelques références

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